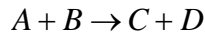


**10.37 HW 3**  
**Spring 2007**

**Problem 1.** A CSTR of volume 0.602 liters (constant density liquid phase) is operated in which the following reaction occurs:

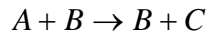


The feed rate of A is 1.16 liters/hr of a solution at concentration 5.87 mmol/L. The feed rate of B is 1.20 liters/hr at a concentration of 38.9 mmol/L. The outlet concentration of species A is 1.094 mmol/L.

Calculate the rate constant for this reaction assuming a mass-action rate law of the form:

$$r = k[A][B].$$

**Problem 2.** Consider the catalyzed reaction:

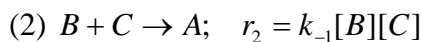
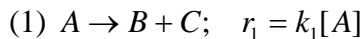


with the second-order rate constant  $1.15 \times 10^{-3} \text{ m}^3/\text{mol}/\text{ksec}$ . The rate law is

$$r = k[A][B].$$

What volume of CSTR would be necessary to give 40% conversion of species A if the feed concentration of A is  $96.5 \text{ mol}/\text{m}^3$ , the feed concentration of B is  $6.63 \text{ mol}/\text{m}^3$ , and the flow rate is  $0.5 \text{ m}^3/\text{ksec}$ ?

**Problem 3.** Two configurations of CSTRs are contemplated for performing reversible hydrolysis of compound A to produce compounds B and C. The forward reaction is pseudo-first-order with respect to A, with rate constant  $k_1 = 1.82 \times 10^{-4} \text{ s}^{-1}$ . The reverse reaction is second-order with rate constant  $k_{-1} = 4.49 \times 10^{-4} \text{ M}^{-1}\text{s}^{-1}$ .

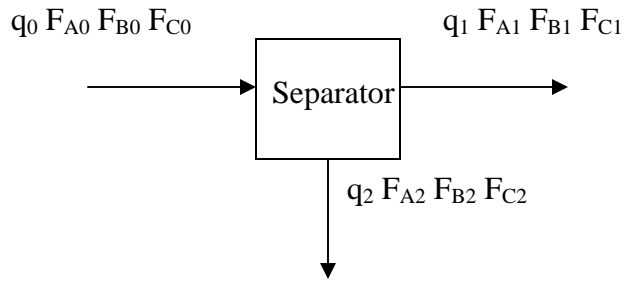


The feed is a dilute aqueous solution of A (concentration 0.25 mol/L) at a rate of 0.25 liters per hour.

Consider the following two configurations:

a) a single 15 liter CSTR.

b) three 5-liter CSTRs in series, with 75% of product species B & C selectively removed between stages 1 and 2 and between stages 2 and 3, with appropriate adjustment in flow rate; the volumetric flow rates in the two streams leaving a separator are proportional to the total number of moles of A, B, and C in each stream. See the separator diagram below.



If  $q$  is the volumetric flow rate and  $F$  is the molar flow rate, then the separator follows the relationships:

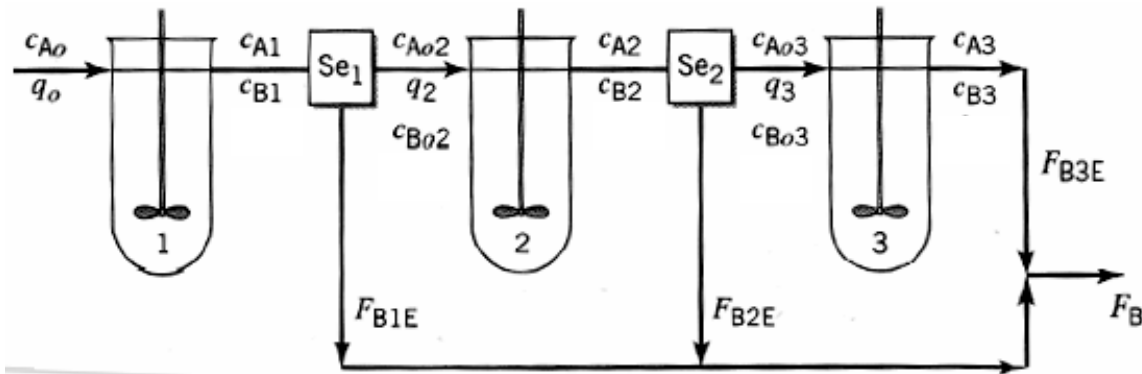
$$F_{A2} = 0$$

$$F_{B2} = 0.75F_{B0}$$

$$F_{C2} = 0.75F_{C0}$$

$$\frac{q_1}{q_2} = \frac{F_{A1} + F_{B1} + F_{C1}}{F_{A2} + F_{B2} + F_{C2}}$$

A full flow diagram is shown below.



Determine the steady-state production of compound B in mol/h for options a) and b).